Useful Calculation sheets (excel and mathcad files) for Design of Above Ground Storage Tanks

If you are intrested to order following files pls send your request to jimallen212@gmail.com

The price for this collection is 50 US\$

ltem no	Title	Filetype
1	API 650- Storage Tank Design Calculation	Excel
2	Floating roof Storage Tank design as per API 650 including bleeder vent, roof drain and wight calculation	excel
3	Design of steel storage tanks- fixed roof with and without column	excel
4	Design Calculasion for fixed cone roof storage tanks	Excel
5	Foundation design of storage tanks	Excel
6	Seismiac base shear and overturning moment calculation for storage tanks	Excel
7	Dike Design for tank farm area	Excel
8	Cathodic Protection design calculations for fuel storage tanks	excel
9	API 650 Base Plate Design	Mathcad
10	API 650 Pipe Column Design	Mathcad
11	API 650 Rafter Design	Mathcad
12	API 650 Bleeder Vent Design	Mathcad
13	API 650 Internal Floating Roof Design	Mathcad
14	Shell Defelection and rotation due to nozzele forcess	excel
15	Basis for nozzle tank load check	Excel
16	Tank Pressure and Vacuum Protection calculation	excel
17	Tank heat loss calculation	excel
18	Material properties as per ASME III.1	excel

FIRST PAGE OF EACH CALCULATION FILES ARE AS BELOW:

Design of Storage Tanks

Tank Sizing

Tank design for Int.Pressure

Wind Analysis

Seismic Analysis

Tank design for External Pressure

Weight Calculation

OutPut

Foundation loadings

Suggestion/Comments

Linde Engineering India Pvt.ltd

Project :	Design of Storage T	Prepared:	
Date ·			Checked: Approved:
Duto .	API 650 11 th Ed.lune	2007.Add-2 Nov 20	09
	Design I	nnut Data	
D	Design Int pressure above atm		(0 psi) $(0 mmWC)$
	Design External pressure	0.0 kra	[Tank need not be designed for Ext Press]
	Design Internal temperature	65.00 °C	
<u> </u>	Design External temperature	03.00 °C	
Te		47.00 C	
		50.0 C	
<u>E</u>		0.85	
D	lank inside diameter	22.0 m	
H2	Height of tank shell	16.0 m	
H	Maximum design liquid level	16.000 m	
Ht	Test Liquid Level	16.000 m	
Vnom	Nominal capacity	6082 m ³	
Vnet	Working capacity	6082 m³	
_	Stored liquid	solution	
G	Specific gravity of the liquid	0.718	
Gins	Specific gravity of Insulation material	0.28	
CA	Corrosion allowance for shell	1.5 mm	
CAb	Corrosion allowance for bottom	0.0 mm	
CAr	Corrosion allowance for roof	0.5 mm	
thins	Insulation thickness	0.0 mm	
	Mate	erials	
		162062 6 *P	Yield Stres: 250 MPa
	Shell Plate	132002GFB	Tensile Stress : 410 MPa
	Poof Plate	IS2062CrB	Yield Stress : 250 MPa
_	Root Flate	132002015	Tensile Stress : 410 MPa
	Pottom Plata	IS2062CrP	Yield Stress : 250 MPa
	Bottom Plate	132002015	Tensile Stress : 410 MPa
	Ton Angle (Stiffners	1520525-0	Yield Stress : 250 MPa
	Top Angle/Stimers	132002015	Tensile Stress : 410 MPa
	Shell cou	rses details	
	Shell Course Numbers	8 N°s	
W ₁	Width of 1 st shell course Bottom	2000 mm	
W ₂	Width of 2nd shell course	2000 mm	
W ₃	Width of 3rd shell course	2000 mm	
W_4	Width of 4th shell course	2000 mm	
W ₅	Width of 5th shell course	2000 mm	
W ₆	Width of 6th shell course	2000 mm	
W ₇	Width of 7th shell course	2000 mm	
W ₈	Width of 8th shell course	2000 mm	Okay
W ₉	Width of 9th shell course	0 mm	

1 .0 DESIGN CODE & SPECIFICATION DESIGN CODE

1.1 TANK

: API 650 11th Edition

	Item number	: 7061T	-3901
	Roof (Open/Close)	: Close	
	Type of roof (Cone-roof / Dome-roof / Flat-roof / NA)	: Floatir	ng Roof
1.2	GEOMETRIC DATA		
	Inside diameter, Di (corroded) (@ 39,000 mm)	=	39,006 mm
	Nominal diameter, Dn (new) (based on 1st shell course)	=	39,028 mm
	Nominal diameter, Dc (corroded) (based on 1st shell course)	=	39,031 mm
	Tank height (tan/tan), H	=	20,700 mm
	Specific gravity of operating liquid, S.G. (Actual)	=	0.790
	Specific gravity of operating liquid, S.G. (Design)	=	1.00
	Nominal capacity, V	=	24736 m ³
	Maximum design liquid level, HL	=	20,700 mm
1.3	PRESSURE & TEMPERATURE		
		(A) A A A	0.00 1

Design pressure: Upper , Pu(Atmospheric) =0.00 mbarg: Lower , Pl=0.00 mbarg VacDesign temperature: Upper , Tu= $70 \ ^{\circ}\text{C}$: Lower , Tl= $-17 \ ^{\circ}\text{C}$

1.4 MATERIAL & MECHANICAL PROPERTIES

Component		Material	Tensile	Yield	Corrosion
			Stress	Stress	Allowance
			St(N/mm ²)	Sy(N/mm ²)	c.a.(mm)
PLATE	_				
Shell Plate	(Mat'l Code # 1) (bot)	A 516 GR. 65N	448.00	241.00	3.000
	(Mat'l Code # 2) (top)	A 516 GR. 65N	448.00	241.00	3.000
Annular Plate		A 516 GR. 65N	448.00	241.00	3.000
Bottom Plate		A 516 GR. 65N	448.00	241.00	3.000
Roof Plate		A 516 GR. 65N	448.00	241.00	3.000
STRUCTURE	MEMBERS				
Roof structure	(rafter,bracing,etc)	A 516 GR. 65N	448.00	241.00	3.00
Top Curb Ang	le	A 516 GR. 65N	448.00	241.00	3.00
Intermediate V	Vind Girder	A 516 GR. 65N	448.00	241.00	3.00

DESIGN OF STEEL STORAGE TANKS AS PER API-650

SELF-SUPPORTED CONE ROOF

DESIGN DATA				
Service		HSD SEF	RVICE	Allowable Design St
Capacity		21 KL		Allowable Test Stre
Type of tank		Self Supported Cone Roof		Specific Gravity of L
Dia of tank (feet)		10.00)4	Corrosion Allowance
Height of tank (fe	et)	9.51	2	
Slope of roof		1:5	5	
Slope of bottom		Flat Bot	ttom	
Plate Data				
Plate width (mete	er)	2.4390		
Plate height (met	er)	1.2195		
Den. of mat. (Kg/	⁷ m ³)	7850		
SHELL				
			By one	foot method. See see
			, 0	n page 3-7 of API - 6
Course #	Lig. height	Height of	Design shell	Design shell
from bottom	in tank	each Course	thickness	thickness
of tank	(H)		(t _d)	(t _d)
	ft	mm	inches	mm
				1
1	9.512	1219.512	0.126	3.211
2	5.512	1219.512	0.123	3.112
3	1.512	460.976	0.119	3.013
Note:	According to se	ec. 3.6.1.1 min. thk.of ta	nk of dia. <50ft sho	uld be 3/16 inches(
Course #	# of full	Size of ful	l plate	# of partial
from hottom	plates in	in each c	ourse	plates in
of tank	shell ner	(Width)	(Height)	shell ner
ortanic		mm	mm	

CONTENTS:-

<u>Sr.No</u> .	DESCRIPTION	PAGE
1	DESIGN DATA	3
2	CALCULATIONS FOR MINIMUM SHELL THICKNESS	4
3	BOTTOM PLATE DESIGN	5
4	INTERMEDIATE WIND GIRDER	
	4.1 AS PER API 650 SEC. 3.9.7	6
5	SUPPORTED CONICAL ROOF	
	5.1 DESIGN OF ROOF PLATE	7
	5.2 DESIGN OF ROOF PLATE WITH STIFFENING	7
	5.3 DESIGN OF COMPRESSION RING	8
	5.4 DESIGN OF ROOF RAFTERS	10
6	COMPRESSION AREA AT ROOF TO SHELL JOINT	
	6.1 DESIGN OF COMPRESSION AREA AS PER API 650 App. F	11
7	STABILITY OF TANK AGAINST WIND LOADS	
	7.1)RESISTANCE TO SLIDING	13
8	FOUNDATION LOADING DATA	14
9	VENTING CALCULATIONS	16
10	NOZZLE FLEXIBILITY ANALYSIS AS PER APPENDIX P	19
11	SHELL TO ROOF RAFTER JOINT STRESS ANALYSIS	20

1) DESIGN DATA

Design Code	:	: API 650, 10th Edition, Add.4 2005, Appendix F					
Client's Specs.	:	32-SAN	ISS-005, BD-40	7062 Rev.	00C		
Fluid	:	FIRE / U	UTILITY / WAS	H WATE	R TANK		
Material	:	SA-516	Gr 70.				
Density of contents	D_L	=	1004.9	kg./m ³			
Specific gravity of contents	G	=	1.0049				
Material's yield strength	dy	=	260	MPa			API 650 Table-3.2
Design Temperature	Т	=	71	°C			
Internal Pressure	Pi	=	0.747	Kpa	=	3.0	inch of water
External Pressure	Pe	=	0.245	Kpa	=	1.0	inch of water
High Liquid Level	H_l	=	8.560	m			
Design Liquid Level	H_L	=	9.000	m			
Allowable Design Stress at Design Temp.	Sd	=	173.00	MPa			API 650 Table-3.2
Allowable Test Stress for Hydrostatic Test Condition	St	=	195.00	MPa			API 650 Table-3.2
Corrosion allowance							
Bottom		=	3.20	mm			
Shell		=	3.20	mm			
Roof		=	3.20	mm			
Roof Supporting Structure		=	3.20	mm			
Slope of Tank Roof	θ	=	9.46	0		1:6	
Outside dia. of tank	Do	=	13.516	m			
Inside dia of tank	D_i	=	13.500	m			
Nominal dia. of tank	D	=	13.508	m	=	44.3	2 ft
Height of Shell	Н	=	9.000	m			
Weight of roof attachments							
(platform, handrail, nozzles, etc.)	Wr	=	30.00	KN			
Weight of attachments (pipe clips, nozzles, etc.)	Ws	=	5.00	KN			
Weight of curb Angle	Wc	=	6.85	KN			
Design Wind Velocity	V	=	154	Km/hr			
Yield Strength of Steel Structure	Fy	=	250	M Pa	=	36.2	6 Ksi
Live Load on roof	L _r	=	1.2	Kpa			API 650 Sec. 3.2.1d

kN

kN

4492.39

250 kPa

4-CALCULATION FOR TANK FOUNDATION Item No.

Refer to Dwg.No. Refer to G.A Dwg No.

Service

Туре

-	
-	

TK-1601 Oily Water Retention Tanks Concrete Ring Wall Foundation

8474L-015-DW-1743-626 RGX-D-87-1354-001

 $: M_S$

LOADING DATA 4.1-

-

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Document

FOUNDATION LOADING

O WEIGHT SUMMARY Dead Load, Shell, Roof, & Ext.Structure Loads : D_L 14.37 Live Load $: L_L$ 2.89 Uniform Load, Operating Condition : Wo 112.89 Uniform Load, Hydrotest Load : W_h 123.93 Base Shear due to Wind : F_w 80.71 Reaction due to Wind : Rw 2.09 Moment Due to Wind : M_w 533.15 Base Shear due to Seismic Load $: F_S$ 807.26 Reaction due to Seismic Load $: R_S$ 17.16

9.000

9.174

12.000

m

m

m



TANK DATA 4.2-

-	Diameter of Tank = D =	
-	Bolt Center Dia = BCD =	

Moment Due to Seismic Load

-	Height of Tank = H^T =
---	--------------------------

MATERIAL SPECIFICATIONS 4.3-

fy	420	MPa
fc'	28	MPa
γ Concrete	24.00	kN/m ³
γ _{Steel}	78.40	kN/m ³
γ _{Soil}	18.00	kN/m ³
γ _{Water}	10.00	kN/m ³

4.4-SOIL CONDITION

Net Soil Bearing Capacity of Area In normal operations

Coefficient of Lateral Soil Pressure

$\varphi =$	30
$Ka = tan^2 (45 - \phi/2)$	0.33
$Ko = 1 - sin\phi$	0.50
$Kp = tan^2 (45 + \phi/2)$	3.00
μ =	0.50
F	$\begin{aligned} &\zeta a = tan^2 \left(45 - \phi/2\right) \\ &\zeta o = 1 - sin\phi \\ &\zeta p = tan^2 \left(45 + \phi/2\right) \\ &\iota = \end{aligned}$

FOUNDATION OUTLINE 4.5-

-

-

-

-	Top of Ringwall	EL +
-	Bottom of Ringwall	EL +
-	Unit Elevation	EL +









m

m



	Tank and Dike Work Book								
	Instructions and Notes								
1	Purpose: This Excel Work Book was created to assist the Plant Layout Designer with a task that can be complicated, filled with potential error and take a lot of time. The goal is to reduce costs by reducing time and improving quality.								
2	Application: This Work Book can be used for single tank within a single containment area or can be used for multiple tanks within a single containment area.								
3	Contents: There are five (5) sheets included. Sheet "1 (this sheet) is the instructions and Notes. Sheet #2 is a list of some of the most common API Storage Tank sizes. Space is included so the user can record other sizes consistent with project specific requirements. Sheet #3 is the work sheet for the Single Tank application. Sheet #4 is the work Sheet for the multiple tank application. Sheet #5 is a two page work sheet: Page 1 is for the Dike Detail and page 2 is for the Tank Pad Detail.								
4	Tank Data: A) Collect a list of Tanks for the Project. This list must include the sizes (in Barrels), the Tank Types and the Commodities. B) Determine if there is a Local or Client imposed Code that defines Grouping or separation of Tank types or Commodities. If there are Tanks on the project list that are not included on Sheet #2 then add them in the "Yellow" spaces provided and in this case only hit "Save".								
5	Civil/Structural Data: Meet with the appropriate Civil/Structural Group and have them define preliminary guidelines for A) the Angle of Repose of the material to be used for the Dikes (Berms, Bungs, etc.), the recommended maximum height of the Dikes and for B) The proposed approach to Tank Pad profiles (Height and configuration).								
6	The Task : Add the Dike Height and Angle of Repose data into Page 1 of Sheet #5. Add the Tank Pad height Data to Page 2 of Sheet #5								
7	For Single Tank Installation: Use Sheet #3. Enter all the data required (and Optional) Data in the "Yellow" user entry boxes. The Form and the built-in formulas will do the work for you.								
8	For Multiple Tank Installation: Use Sheet #4. Enter all the data required (and Optional) Data in the "Yellow" user entry boxes. The Form and the built-in formulas will do most of the work for you. With this grouping you must select and enter a choice for the "Width" of the Containment Area. This is a "Trial and Error" method until you get the shape that fits the project needs.								
9	Quitting and Closing: It is recommended that before closing the program that Copies of all Sheets be printed out for all Tank configurations completed. When closing the program do not save the data. This will allow you to start with a clean Work Book for the next Tank configuration.								
e:	Each Sheet of this Work Book is Password protected. In order to make a change to a "cell" that is not "Yellow" the Sheet must be "unprotected" using the password. This Password will be furnished on request.								

Note:



MOGAS Tank For Fuel Point		
Data		
Physical Dimensi	ons	
Length	4	13.12
Hight	1.5	4.92
Width	2.25	7.38
Diameter		(
Structure Specs	•	
material Type	Steel	
Shape	Rectangular	Prism
Elyctrolyte		Soil
Electrolyte Resistivity	5000	ohm-centimeter
Current		
Current Requirement	1	milli Amp
Total Current Requirment	0.3953712	Amp
Coating Resistance		
Resistance	2500 ohm pe	r square foot
Life Time		
Years	2	0
Efficiency		
Percentage	8	0
Anode Type	magnisium A	lloy Anode
Tank Surface Area	26.7	5 m^2
	30.7	
Tank Surface Area	395.371	2 m^2

Anode Specification					
Dimensions	3.7	3.75x3.75 x26			
Weight 17 lb					
Package Weight	45 lb	45 lb			
Package Size	6.5 x 29				

,

Design Steps								
Soil Resistivity								
	Selecting	Anode						
Number of Anod	es meets Grou	, undbed resistanc	e Limitations					
Number	of Anodes for	Sys life expecta	incy					
N	umber of Ano	des to be used	,					
	Select Groun	dbed layout						
	Number o	of Anode						
Y x S x I								
w =		E						
		-						
w =	Waight		lb					
Y =	Years		20					
=	Current Requ	iirement	0.3953712					
S =	pound per Ampere-year 8.8							
E =	years 20							
W=	86.981664							
No of Anodes	5.1165685	6						

Design For Obove-Ground Fuel Tank

Baseplate Design per API 650

A. Introduction

API 650 requires that the baseplates be designed per AISC or other approved standard. These baseplates are designed using the latest edition of AISC with temperature modification factors per API 650, Appendix M.

B. Geometry



Pipe Column Design per API 650

A. Introduction

API 650 requires that the columns be designed per AISC or other approved standard. These columns are designed using the latest edition of AISC with temperature modification factors per API 650, Appendix M.

B. Geometry



Rafter Design per API 650

A. Introduction

API 650 requires that the structural rafters be designed per AISC or other approved standard. These rafters are designed using the latest edition of AISC with temperature modification factors per API 650, Appendix M. API 650 requires that rafters not use roof plate for lateral support when considering the roof plate loads only. When considering the total load with live load and other dead loads included, the roof plate may be considered as effective in bracing the compression flange of the rafter (per API 650).

B. Geometry Beam Selection (W or C shapes) W12X16 / W310X23.8 W5X16 / W130X23.8 Internal Rafter W6X16 / W150X24 W10X17 / W250X25.3 C External Rafter Radius to outside rafter Radius to inside rafter Number of lateral Number of rafters in bay connection connection braces $R_0 := 50 f$ $R_1 := 4 \cdot ft$ $N_{rb} := 50$ Npt := Roof slope Thickness of roof Effective Span of rafter RS := .75 t_r := .1875 In $L_{B} := R_{0} - R_{I} = 46.00 \text{ ft}$ C. Material Properties Yield Strength Safety factor required per AISC 360 F_{VB} = 50 ks $\Omega_{b} := 1.67$ Rafter Design (AISC 360-05) D. Rafter Loadings Ground snow load Balanced snow load on roof SLa = 25 psf SLb = 0.84 SLa = 21.00 psf Addițional roof dead load Roof live load DLmisc := 1.5 psf $LL_r := 20 \text{ ps}$ External pressure Design temperature T_d ≔ 350 °F Pext = 5.2 psf



Internal Pontoon Floating Design

A. Introduction

This program designs pontoon floating roofs to the requirements of API 650, Appendix H (internal roofs)

Design methodologies are as follows:

 Pontoon ring is designed using section properties determined in accordance with the AISI Cold-Formed Steel Design Manual (accounts for local buckling of plates with large width to thickness ratios)
Floating roof legs are designed in accordance with AISC 360, Latest Edition for loads listed in API 650, Appendix H.

3. Deck stresses and deflections are determined in accordance with the paper: "Stresses in Ruptured Floating Roofs", H.I. Epstein and J.R. Buzek, 1978 ASME Journal of Pressure Vessel Technology.

4. Pontoon ring is modeled as a ring on elastic foundation.

5. Ponton ring strength is evaluated in accordance with AISI Cold-Formed Steel Design Manual.

B. Pontoon Geometry



BASIS FOR TANK NOZZLE LOAD CHECK AS PER API650-P3

AT NOZZLE OF D-002 LOAD CASE OPER. AT MAX. DESIGN TEMP.

INPUT

1)	GEOMETRICAL	INPUT

TANK DIAMETER, D =	32020	mm
TANK SHEEL THICKNESS, ts =	10	mm
NOZZLE OUTSIDE DIAMETER, d =	168.275	mm
NOZZLE NECK THICKNESS, tn =	12.7	mm
REINFORCEMENT PAD THICKNES, tr =	12.7	mm
NOZZLE LOCATION FROM BOTTOM, I =	275	mm
MATERIAL =	A36	
ALLOWABLE DESIGN STRESS, Sd =	160	MPa
2) LOAD INPUT		
2a) SUSTAINED LOAD		

44 N	RADIAL THRUST, F _R =
-30 N	TRANSVERSE SHEAR FORCE, V _C =
<mark>-958</mark> N	LONGITUDINAL SHEAR FORCE, V _L =
5.30E+04 N-mm	TORSIONAL MOMENT, M_T =
1.00E+03 N-mm	CIRCUMFERENTIAL MOMENT, M _C =
-1.10E+04 N-mm	LONGITUDINAL MOMENT, M

2b) THERMAL LOAD

<mark>-8761</mark> N	RADIAL THRUST, F _R =
<mark>1479</mark> N	TRANSVERSE SHEAR FORCE, V_c =
<mark>3793</mark> N	LONGITUDINAL SHEAR FORCE, V_L =
-1.98E+06 N-mm	TORSIONAL MOMENT, M_T =
2.77E+05 N-mm	CIRCUMFERENTIAL MOMENT, M _C =
8.61E+06 N-mm	LONGITUDINAL MOMENT, M_L =

CALCULATION FOR GEOMETRIC

u =	(d/D) x (D/t) ^{0.5}	
	0:20	
d/tn =	13	
R =	2(Dxt) ^{0.5}	
D -	1705	
h =	L/B	
	0.16	
t/tn =	1.787401575	
7 =	(h+0.5)/1.5	from Fig. P-11
2 -	0.66	

STRESS FACTOR

Based on d/tn & t/tn user need to do interpolation as per the appropriate table attached

LOAD	STRESS FACTOR	VALUE
FR	f _r	2.24293374
FR	f _θ	1.304759646
MC	f _r	1.649571821
MC	f _θ	1.171710421
ML	f _r	1.63916237

Produc	ct Form	l										Remarks:
🔘 Plat	te	Select	first		TABLE 1A							
⊖ Forg	gings	the Pro	oduct		MAXIMUM	ST	RESS VALUES	5 <u>5</u> FOR		5		
○ Pipe	e	Form b	oefore		FERROUS M	IATERIALS AT	[D]	ESIGN TEMPI	ERATURE	4		
🔿 Tube	Э	looking	ooking for (Materials Permitted on ASME Se					Sec. VIII-1 Only	v)	iter C		
O Bar		the ma	terial		X			•••••••••••••••••••••••••••••••••••••••	, ,	u	1	
O Fitt	ting	specifi	cation.		ASME	2001		Allowable	e Stress at D	esian Ter	np.	
O Cast	t8	-1			Design Ter	nperature		Stress	16.7	115.14	1174.1	
		Plate			90 °C	194 °	F		ksi	Мра	kg/cm ²	
SA-204		•	316H	▲					Mi. Streng	yth		
SA-225			316H		Nominal	Composition		Tensile	70	482.63	4,922	
SA-240			316L 316I		16Cr -	12Ni - 2Mo		Yield	25	172.37	1,758	Heat-Resisting Stainless
SA-285			316LN	▼								SteelLow Carbon
Spec I	No		Type/C	Grade	Alloy De	esign / UNS		Applic. &	Max. Temp	.(deg.F/N	IP)	REMARKS; *1) Rimmed Steel
SA-24	0		31	6L	S	31603		Limits on Se	ction I	85	50	ASME SEC.II SA-6/SA-6M
ASME I	Locator							Limits on Se	ction II	80	00	para.3.6-Steel containing
Add	enda	Page	Line		Class / C	ond / Tempe		Limits on Sec.VIII-1 850		evolution of carbon monoxide		
0)1	66	11			•						while the ingot is solidifying,
Applica	able No	otes			-			Ext.Chart.No.	Tick(in)	P-No.	G-No.	resulting in a case or rim of
G5	G42							HA-4	0	8	1	
SCROL	L DOW	/N to vie	w Notes	s or use "	FIND" {Ctrl.+F}	command in "I	EDI	T" menu.				
Genera	al Notes	5										
(a)	The fo	llowing a	abbrevia	tions are u	ised: Applic., A	pplicability; Con	d., (Condition; Desig	g., Designati	on; Smls.,	Seamles	ss; and Wld., Welded.
(b)	The str	ess value	es in this	s Table ma	ay be interpolate	ed to determine v	alue	es for intermedia	te temperatu	ires.		
(c)	(c) When used for Section III Class MC design, the stress values listed herein shall be multiplied by a factor of 1.1 (NE-3112.4); these values shall be											
	conside	ered as d	esign str	ress intens	ities or allowab	le stress values a	s re	quired by NE-32	200 or NE-3	300, resp		
(d)	(d) For Section VIII applications, stress values in restricted shear such as dowel bolts or similar construction in which the shearing member is so restricted that											
	the sec	tion und	er consid	deration w	ould fail withou	it reduction of ar	ea s	hall be 0.80 tim	es the va			
(e)	For Se	ection V	III appli	cations, s	stress values i	n bearing shall	be	1.60 times the	values in th	he above	Table.	

(f) Stress values for -20 to 1000F are applicable for colder temperatures when toughness requirements of Section III or Section VIII are met.

G5 Due to the relatively low yield strength of these materials, these higher stress values were established at temperatures where the short time tensile properties govern to permit the use of these alloys where slightly greater deformation is acceptable. The

G42 For Section I, use is limited to PEB-5.3. See PG-5.5 for cautionary note.

Ambient Heat Loss from a Vessel

This tool calculates the ambient heat losses from a vertical vessel.

Vessel Dimensions

Tank diameter	(ft)	50
Vessel height	(ft)	48
Liquid height	(ft)	30
Sidewall insulation thickness	(inches)	1.5
Roof insulation thickness	(inches)	0

Ambient Conditions

Ambient temperature	(°F)	35
Wind speed	(mph)	10

Liquid Properties

Temperature	(°F)	55
Liquid specific heat	(BTU/lb/°F)	0.6
Liquid viscosity	(Centipoise)	40
Liquid thermal conductivity	(BTU/hr/ft/°F)	0.12
Liquid density	(lb/ft ³)	46.8
Liquid coeff of thermal expansion	(/°F)	1.00E-06

Vapor Properties

Vapor specific heat	(BTU/lb/°F)	0.25
Vapor viscosity	(Centipoise)	0.0175
Vapor thermal conductivity	(BTU/hr/ft/°F)	0.015
Vapor density	(lb/ft ³)	0.08
Vapour coeff of thermal expansion	(/°F)	0.002

RESULTS		
	Area	Heat Loss
Location	(ft²)	(BTU/hr)
Dry Wall	2,827	6,320
Wet wall	4,712	18,130
Roof	1,967	2,717
Bottom	1,963	1,157
Total	11,471	28,324

Yellow fields are input

Red fields are results

* These calculations are provided for educational use only - USE AT YOUR OWN RISK.

Assumptions

- 1. Roof slope = 0.75 inch/ft
- 2. Thickness of metal sidewalls and roof = 0.1875 inches
- 3. Thermal conductivity of metal sidewalls and roof = 26 BTU/Hr-ft-°F
- 4. Insulation Type = cellular glass
- 5. External surface has white paint with emmissivity = 0.9
- 6. Dirt factor for dry sidewall = 0.001 ft².hr.°F/BTU
- 7. Dirt factor for wet sidewall = 0.00125 ft².hr.°F/BTU
- 8. Dirt factor for bottom = $0.002 \text{ ft}^2.\text{hr.}^\circ\text{F/BTU}$
- 9. Dirt factor for bottom = 0.002 ft².hr.°F/BTU
- 10. Dirt factor for roof = 0.001 ft².hr.°F/BTU
- 11. Atmospheric pressure = 14.7 psia
- 12. Ground Temperature = 5°F above ambient temperature
- 13. Thermal Conductivity of ground = 0.8 BTU/Hr/ft/°F
- 14. Specific heat of air = 0.25 BTU/lb/°F
- 15. Viscosity of air = 0.0175 Centipoise



Tank Pressure & Vacuum Protection Design Sheet

Tank_____

Crude Oil

Stored Material

Flash Point	°F	350	(Estim.)	MAWP
Boiling Point	°F	360	(Estim.)	Max Vacuum
Latent Heat Vap.	Btu/lb	144	(Hexane)	Diameter
Molecular Wt.		274		Max fill Height
				Max fill Volume
Inflows, SCFH				Wetted Area
Normal Operation		12,861		
Relief Scenario		20,578	Fire	Therm. Conductivity
				Required Capacity
Outflows, SCFH		40,104		
			Blow Through	From Upstream
Breathing, Note 1	-			From Hose
Out	SCFH	6,295		Relief, Hose +unload
In	SCFH	10,491		
			O C C C C C C C C C C	
Vent Valve set at	4	in WC	Consider this when usi	ng emission vapor contro
Required	SCFH	NA	Normal max inflow + ou	It breathing + Blowoff (no
selected	SCFH	NA	With vent system Press	sure Drop of 9 in WC
Fail Open	SCFH	0	Consider this only if the	e tank vents to a vacuum
Blankot Gas Valvo so	t at 2" \N/	c		
Required	SCEH	50 505	sum of outflows + in Br	eathing + fail open vent v
Selected	SCEH	75 803	Fisher Model Reg	lator with " trim
Valve Eail Open	SCITI SCILI	75,095	This flowrate assumes	the value's Cy determined
	30111	U		
Prossura Raliaf Casa	6			
Inflow	SCEH	102 766	Relief Inflow + Out Bre	athing + Blanket Gas Valv
Fire	SCFH	877.654	Fire + Blanket Gas valve	
Outflow	SCFH	50.595	5 sum of outflows + in Breathing + fail-open yent y	
Conservation Vent				
Pressure side set a	t	5	in WC, Rated at	20 in WC
Required	SCFH	0	zero (if have Vent Valv	e and Emergency vent) o
Selected Size	SCFH	44,000	each from catalog; tota	I number 1
Vacuum Sid	e set at ().5 oz/in ² Vacuu	m. rated at 2 1/2	oz/in ²
Required	SCFH	50.595	Outflow Case	
Selected Capacity	SCFH	15.000	each from catalog: tota	I number 1
	••••	,		
Emergency Relief, No	te 2			
Set at	10	in WC, Rated a	at 20	in WC
Required	SCFH	833,654	zero (if Con vent has c	apacity) or Worst case - C
Selected Size	SCFH	680,000	each from catalog; tota	I number 1
		,	3 ,	
Selected Equipment:		Tag	Manufacturer	Model
Blanket Gas Regula	ator	PCV 400B	Fisher	1190
Biannot Guo riogui				1100
Conservation Vent		PVSV 400		
Emergency Vent				
Notes:				

1) For Tanks larger than 840,000 gal (20,000 Bbls), refer to API-2000 for breathing requirement